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A Comparative Study of State-of-the-Art Meshless Methods for Flow and Transport Simulation in Porous Media

T. I. Eldho^{1,*}, Sanjukta Das¹, Aatish Anshuman² and Tinesh Pathania³

¹Department of Civil Engineering, Indian Institute of Technology Bombay, Mumbai, Maharashtra, India

²Department of Civil Engineering, School of Infrastructure, Indian Institute of Technology Bhubaneswar Argul, Khordha, Odisha, India

³Department of Environmental Science and Engineering, Indian Institute of Technology (Indian School of Mines), Dhanbad, Jharkhand, India

*Corresponding Author: T. I. Eldho. Email: eldho@civil.iitb.ac.in

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ABSTRACT: In recent years, meshless methods have been increasingly applied to the simulation of various engineering problems due to their inherent advantages over traditional mesh-based approaches, including greater flexibility, independence from predefined meshing, simpler adaptive analysis, improved automation, and suitability for complex problems. Several meshless methods have been used for porous media simulation, and are broadly categorized into collocation, global weak form and local weak form methods. In this study, a comprehensive comparison of the applicability of these three categories of meshless methods for simulating coupled flow and transport problems in porous media is presented. The Radial Point Collocation Method (RPCM) (strong form), the Element Free Galerkin Method (EFGM) (global weak form) and the Meshless Local Petrov Galerkin (MLPG) method (local weak form) are implemented and systematically compared. These methods are applied to the analysis of flow in a synthetic regular domain aquifer, flow and non-reactive contaminant transport in a synthetic irregular boundary porous media problem and groundwater flow in a field aquifer located in India. The simulated groundwater heads are compared with analytical solution, observed field data and results obtained from widely used MODFLOW-MT3DMS models. The deviation of the solutions from the analytical solution is in the range of 0.67% to 0.16% for the hypothetical case study. For the field-scale case study, mean absolute error of 0.183%, 0.181% and 0.188% are obtained for the RPCM, EFGM and MLPG models, respectively, outperforming MODFLOW, which exhibits a deviation of 0.254% from observed values. Overall, the present study reaffirms the practical applicability of these meshless methods for real-world groundwater problems and provides valuable insights into the utilization of each category of meshless method, with respect to problem type, computational efficiency and accuracy requirements.

KEYWORDS: Meshless methods; groundwater flow; contaminant transport; radial point collocation method; element free Galerkin method; meshless local Petrov Galerkin method

1 Introduction

The simulation of groundwater flow and transport is one of the most important porous media problems dealing with large-scale complex aquifer systems. In groundwater problems, the decline in groundwater levels and depletion of groundwater quality are the inevitable consequences of population growth and increasing variability in climatic and precipitation patterns [1,2]. The associated challenges include lowering groundwater table and subsequent drying up of aquifers, reduced discharges to surface water systems,

increased salinization, crop deaths and wider spread of pollution [3]. The estimation of spatio-temporal variations of contaminants combined with head changes in the aquifer aids in effective groundwater management plans [4]. Numerical models are extensively used for the assessment and prediction of aquifer behavior [5].

The Finite Difference Method (FDM) and the Finite Element Method (FEM) are among the most widely used numerical techniques in groundwater simulation. Prominent software packages such as MODFLOW [6], MT3DMS [7], SEAWAT [8], MODFLOW-SURFACT [9], and Parameter ESTimation (PEST) [10] are based on the FDM. FEM-based software includes FEFLOW [11] and SUTRA [12]. Despite their broad applicability, these methods have several limitations such as high cost and memory requirements for meshing and remeshing, difficulty in controlling accuracy, misalignment of mesh with problem boundaries, slower simulation speeds, complex preprocessing and reduced accuracy for higher dimensions and advection-dominant problems [13–16].

To overcome the limitations of the mesh-based methods and the development of more powerful tools, meshless methods were first introduced in 1970s [17]. Since 1990s, several meshless methods have been developed and successfully applied for various Partial Differential Equations (PDEs). Based on the formulation of the PDE, the meshless methods can be classified into strong or weak form methods. Collocation or strong form methods employ a collocation technique for the discretization of the governing PDE, and they are simple, truly meshless and computationally efficient [18], though they may suffer from stability issues at Neumann boundaries. On the other hand, weak or integral forms of governing equations are discretized in weak form methods, and these methods have high stability at Neumann boundaries due to the integration process [17]. The weak form methods are further classified as global or local weak form methods according to the utilization of global domain or overlapping local support domains for the integration purpose [13]. Global weak form methods require a background mesh for integration, and hence they are not truly meshless, while local weak form methods, though truly meshless, are typically more computationally intensive [17].

Among the earliest applications of meshless methods in groundwater flow modelling, is the Element Free Galerkin Method (EFGM), a global weak form method [19–21]. Variants of the classical EFG formulation have been developed to enhance the computational efficiency and numerical robustness. For example, complex variable element-free Galerkin method employs complex variable theory to improve the treatment of two-dimensional field problems and reduce the computational complexity [22]. Collocation techniques using Radial Basis Functions (RBF) are applied for transport simulation [23] and unsaturated zone problems [24]. Local Radial Point Interpolation Method (LRPIM) is employed for coastal aquifer flow modelling [25], and Smooth Particle Hydrodynamics (SPH) is applied for modelling contaminant transport in heterogeneous aquifers [26]. In addition, the Generalized Finite Difference Method (GFDM), which constructs local weighted approximations of differential operators over scattered nodes [27–29], has been successfully applied to diffusion and convection–diffusion problems relevant to porous media flow. Meshless formulations based on finite volume concepts, often referred to as extended or meshless finite volume methods (EFVM/MFVM), have also been developed to preserve local mass conservation while retaining geometric flexibility [30,31]. Furthermore, dimension-splitting meshless methods have been introduced to improve computational efficiency by decomposing multidimensional problems into sequential one-dimensional approximations while maintaining solution accuracy [32].

The adoption of meshless methods in groundwater modelling has been increased since 2010. Meenal and Eldho [33] demonstrated the effectiveness of Point Collocation Method (PCM) for the flow simulation in unconfined aquifers, noting excellent similarity of PCM head computations with the solutions of FEM and Boundary Element Method (BEM). However, PCM has a limitation of high sensitivity to the time step and

shape function parameters. Kovářík and Mužík [34] utilized the local boundary integral method (LBIEM) for density driven flow estimation and proved that the approximation using RBFs can reduce the computational expense. Li et al. [29] further modelled the density driven flows using generalized finite difference method (GFDM), along with implicit Euler and Newton-Raphson methods to benchmark problems. Swathi and Eldho [35] employed the Meshless Local Petrov Galerkin (MLPG) method, a local weak form method for flow simulation. MLPG was found to be a promising tool, with excellent similarity with PCM and BEM and with better stability. The Radial Point Collocation Method (RPCM) is another widely used meshless method for groundwater flow and transport simulations [36]. Patel and Rastogi [37] validated Kansa's RBF-based meshless method for field-scale aquifer simulations. Pathania et al. [38] applied EFGM to model spatio-temporal variations of river-aquifer interactions. Anshuman and Eldho [39] extended RPCM for flow and transport of multiple species with linked first-order reactions. Swetha et al. [40] used LRPIM for flow simulations in confined aquifers and verified the model with benchmark problems. The good agreement of LRPIM with FDM and FEM reiterates its use as an alternative modelling tool. Das and Eldho [41] proposed a hybrid meshless weak strong (MWS) form method by integrating MLPG and RPCM, achieving accurate solutions with less computational effort.

This study presents a systematic and formulation-oriented comparison of three representative meshless methods for groundwater flow and contaminant transport simulations. Rather than comparing algorithms arbitrarily, the selected methods are deliberately chosen to represent the three principal theoretical frameworks in meshless discretization: strong form, global weak form, and local weak form. Primary objective of the study is to evaluate and compare the numerical accuracy, stability, and practical applicability of three representative categories of meshless methods for groundwater flow and contaminant transport problems, using both synthetic and field-scale case studies. The strong form RPCM [36,42], global weak form EFGM [43,44] and the local weak form MLPG [35,45] methods have been applied for solving the groundwater flow equation in unconfined aquifers coupled with the transport of dissolved non-reactive contaminants. The weak-form meshless methods, MLPG and EFGM, have enhanced numerical stability through integration of the governing equations, but at the cost of increased computational effort. In contrast, RPCM is simpler and computationally efficient, but it may be unstable for complex problems. The background integration strategies also differ between EFGM and MLPG. EFGM relies on a background mesh for numerical integration, whereas MLPG employs local subdomains for integration, making it truly meshless and more flexible.

Based on the theoretical distinctions of the three proposed methods, the study is guided by three working hypotheses. First, local weak-form MLPG is expected to exhibit improved numerical stability compared to the strong-form RPCM. Second, global weak-form EFGM is anticipated to provide higher accuracy at the expense of increased computational cost relative to collocation-based approaches. Third, all three meshless methods provide an easy option for varying nodal distribution of computational domain and representing complex boundaries, while achieving better performance compared to the standard grid-based MODFLOW-MT3DMS model. In this study, the meshless models are compared with MODFLOW-MT3DMS simulations in cases where real data or analytical solutions are unavailable. As MODFLOW-MT3DMS is widely used in industries, it serves as a reference for demonstrative comparison and consistency verification. Initially, the models are demonstrated using hypothetical case studies with regular and irregular boundaries, and the deviation of heads and concentrations from RPCM, EFGM and MLPG from analytical solution, MODFLOW and MT3DMS solutions are reported. To further test the realistic application, the three meshless models have been applied to the case study of a real aquifer in Telangana, India, and the flow model results are compared with observed groundwater head data and MODFLOW. Thus, this study provides an in-depth evaluation

of the strengths and limitations of different meshless methods and establishes their practical utility in the field-scale groundwater modelling.

2 Governing Equations

The governing PDE for a heterogeneous, anisotropic unconfined aquifer is given by [6]:

$$\frac{\partial}{\partial x} \left(K_x h \frac{\partial h}{\partial x} \right) + \frac{\partial}{\partial y} \left(K_y h \frac{\partial h}{\partial y} \right) = \left(S_y \frac{\partial h}{\partial t} \right) \pm Q - q \quad (1)$$

where, x and y are Cartesian coordinates, h is the unknown groundwater head, S_y is the specific yield, K_x and K_y are hydraulic conductivities, Q represents the point source/sink, δ is Dirac delta function, q is known domain inflow and t is time. The initial condition is given by [6]:

$$h(x, y, 0) = h_0(x, y, 0) \quad (x, y) \in \Omega \quad (2)$$

where, Ω is the flow domain, $h_0(x, y, 0)$ is the initial head at time $t = 0$. In mathematical form, the boundary conditions can be expressed as [6]:

$$h(x, y, t) = h_1(x, y, t) \quad (x, y) \in \Gamma_1 \quad (3)$$

$$K_n \frac{dh}{dn} = f_1(x, y, t) \quad (x, y) \in \Gamma_2 \quad (4)$$

where Γ_1 is the Dirichlet boundary, n may be x or y and Γ_2 is the Neumann boundary.

The governing advection-dispersion equation in two-dimensions for the non-reactive contaminant transport can be written as [7]:

$$\frac{\partial}{\partial x} \left(D_{xx} \frac{\partial c}{\partial x} \right) + \frac{\partial}{\partial y} \left(D_{yy} \frac{\partial c}{\partial y} \right) - \frac{\partial(v_x c)}{\partial x} - \frac{\partial(v_y c)}{\partial y} = \frac{\partial c}{\partial t} \quad (5)$$

where, D_{xx} is the longitudinal dispersion coefficient, D_{yy} is the transverse dispersion coefficient, v_x , and v_y are the average linear velocities, and c is the dissolved contaminant concentration. The initial conditions and Dirichlet and Neumann boundary conditions are [7]:

$$c(x, y, 0) = c_0(x, y, 0) \quad (x, y) \in \Omega \quad (6)$$

$$c(x, y, t) = c_1(x, y, t) \quad (x, y) \in \Gamma_1 \quad (7)$$

$$D_{xx} \frac{\partial c}{\partial x} n_x + D_{yy} \frac{\partial c}{\partial y} n_y = f_2(x, y, t) \quad (x, y) \in \Gamma_2 \quad (8)$$

where, c_0 is the initial concentration, c_1 and f_2 are the Dirichlet and Neumann boundary values, respectively. The average linear velocities in two-dimensions v_x and v_y are obtained using Darcy's law as:

$$v_x = -K_x \left(\frac{\partial h}{\partial x} \right) \text{ and } v_y = -K_y \left(\frac{\partial h}{\partial y} \right) \quad (9)$$

Further, the dispersion coefficient D_{xx} and D_{yy} can be computed as [7]:

$$D_{xx} = \frac{\alpha_L v_x^2 + \alpha_T v_y^2}{|\mathbf{v}|} \text{ and } D_{yy} = \frac{\alpha_L v_y^2 + \alpha_T v_x^2}{|\mathbf{v}|} \quad (10)$$

where, $|\mathbf{v}| = \sqrt{v_x^2 + v_y^2}$.

Here, α_L and α_T are the dispersivity values in the longitudinal and transverse directions.

3 Meshless Methods

3.1 Overview

The FDM/FEM based models require the discretization of the problem domain into a grid/mesh, with pre-defined connectivity essential for interpolation. Any significant change in external stress conditions or the need for improved accuracy necessitates remeshing, which makes these methods cumbersome. In contrast, the interpolation in meshless methods is performed by the construction of shape function representing heads or concentrations at nodes, inside and on the support domain. In this study, RPCM, EFGM and MLPG models employ Multi-Quadric Radial Basis Function (MQ-RBF), Moving Least Squares (MLS) and Improved Interpolating Moving Least Squares (IIMLS) techniques for the generation of shape functions. The detailed methodology of these approximating techniques is available in [17,46].

RPCM involves collocating the governing equations at nodes and utilizing RBFs for interpolation. It is truly meshless and generates a banded system matrix, making it simple, flexible, and computationally efficient for a wide range of problems. However, RPCM may experience stability issues near Neumann boundaries and require special handling. EFGM, on the other hand, has better stability and a higher convergence rate than RPCM. However, it is not truly meshless and requires a background mesh for the global integration [47]. MLPG is versatile and is truly meshless. The numerical integration in MLPG is performed over small, localized regions, known as integration of sub-domains which are considered as circles centered at nodes [48]. A typical discretization using FDM and three types of meshless methods is illustrated in Fig. 1.

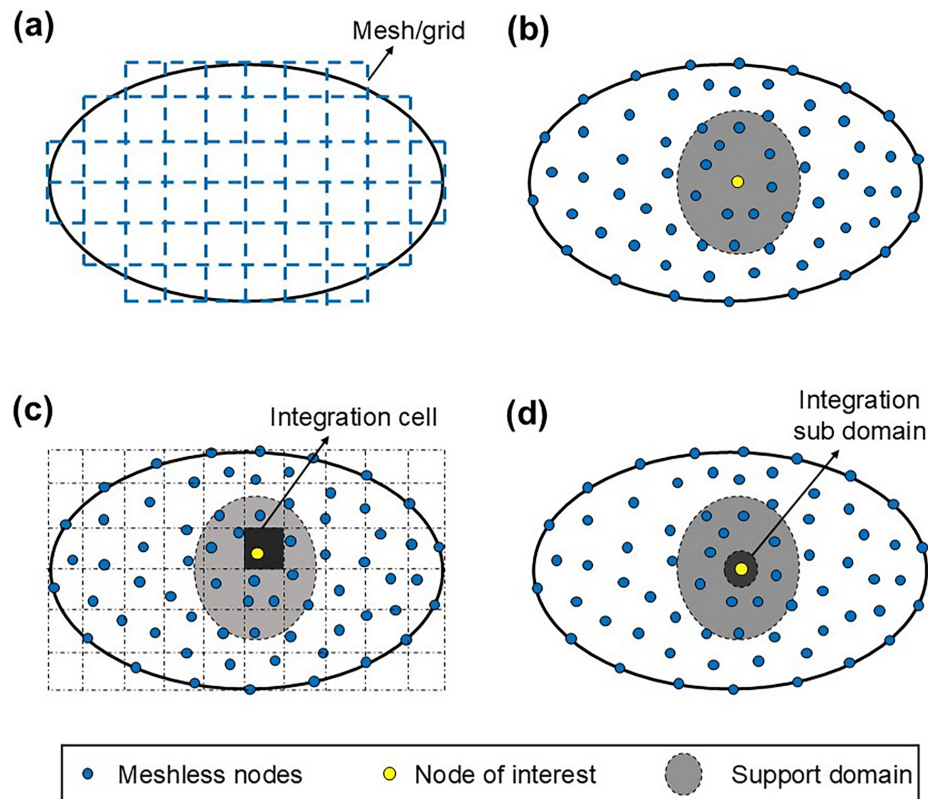


Figure 1: Typical discretization of domain using (a) FDM, (b) RPCM, (c) EFGM and (d) MLPG.

3.2 RPCM Formulation

RPCM employs Radial Basis Functions (RBFs) for shape functions (ϕ) construction. Instead of a predefined mesh, the domain is represented by scattered nodes. Each node is associated with a local support domain, within which the shape function is calculated. These local support domains overlap and collectively cover the entire problem domain. Their shape can vary, but in this work, circular support domains are specifically chosen. The size of each support domain is defined relative to the nodal spacing d_c , typically expressed as a multiple of d_c . The MQ-RBF used for the interpolation is given by:

$$R_i(x, y) = (r_i^2 + (\alpha \times d_c)^2)^q \quad (11)$$

here $r_i = \sqrt{(x - x_i)^2 + (y - y_i)^2}$ where (x, y) is nodal location and (x_i, y_i) are the coordinates of nodes within the support domain. In the MQ-RBF method, q and α are shape parameters. According to Liu and Gu [17], setting q to either 0.98 or 1.03 yields accurate results in both structural and fluid mechanics applications. This study adopts $q = 0.98$, as it has demonstrated good performance in groundwater modelling [36,39]. The sensitivity of the method to the parameter α has been examined in various studies [33,36,39]. The trial solution for h at x_i is computed using n nodes in support domain, as expressed in Eq. (12) [17]:

$$h(x_i) = \sum_{k=1}^n f_{R_k}(x_i, x_k) \cdot a_k \quad (12)$$

Here, f_R is the MQ-RBF, which is given as:

$$f_R(x_i, x_k) = \left[(\|x - x_k\|)^2 + (\alpha \cdot d_c)^2 \right]^q \quad (13)$$

The term $\|x - x_k\|$ denotes the Euclidean distance between x_i and x_k and d_c represents the average nodal spacing. The unknown coefficients a in Eq. (12) is determined by enforcing the MQ-RBF moment matrix to interpolate the nodes within the local support domain [17]:

$$\{a\}_{k \times 1} = \begin{bmatrix} f_R(x_1, x_1) & \cdots & f_R(x_1, x_k) \\ \vdots & \ddots & \vdots \\ f_R(x_k, x_1) & \cdots & f_R(x_k, x_k) \end{bmatrix}^{-1} \cdot \{\hat{h}\}_{k \times 1} = G^{-1} \cdot \{\hat{h}\}_{k \times 1} \quad (14)$$

Here, \hat{h} represents the approximated value of h . Substituting Eq. (14) into Eq. (12) yields the solution for h and can be written as:

$$h(x_i) = \{f_R\}' \cdot [G]^{-1} \cdot \{\hat{h}\} = \{\phi\} \cdot \{\hat{h}\} \quad (15)$$

The term ϕ denotes the shape function, computed for each node within its local support domain. Its directional derivatives are obtained by replacing the MQ-RBF vector (f_R) in Eq. (14) with equivalent derivative terms. Thus, the RPCM solution to Eq. (1) is expressed as shown in Eq. (14). Since the PDE is nonlinear in h , it is approximated following [33], with a semi-implicit scheme used for head discretization:

$$\begin{aligned} & \left[\frac{S_y}{\Delta t} - \theta \left[K_x \left\{ \frac{\partial \phi}{\partial x} \cdot h^t \cdot \frac{\partial \phi}{\partial x} + \phi \cdot h^t \cdot \frac{\partial^2 \phi}{\partial x^2} \right\} + K_y \left\{ \frac{\partial \phi}{\partial y} \cdot h^t \cdot \frac{\partial \phi}{\partial y} + \phi \cdot h^t \cdot \frac{\partial^2 \phi}{\partial y^2} \right\} \right] \right] \cdot \{h^{t+1}\} \\ & = \left[\frac{S_y}{\Delta t} + (1 - \theta) \cdot \left[K_x \left\{ \frac{\partial \phi}{\partial x} \cdot h^t \cdot \frac{\partial \phi}{\partial x} + \phi \cdot h^t \cdot \frac{\partial^2 \phi}{\partial x^2} \right\} + K_y \left\{ \frac{\partial \phi}{\partial y} \cdot h^t \cdot \frac{\partial \phi}{\partial y} + \phi \cdot h^t \cdot \frac{\partial^2 \phi}{\partial y^2} \right\} \right] \right] \cdot \{h^t\} \\ & + q \neq Q \end{aligned} \quad (16)$$

Similarly, the contaminant transport equation (Eq. (4)) can be discretized as follows:

$$\begin{aligned} & \left[\frac{1}{\Delta t} - \theta \left[D_{xx} \frac{\partial^2 \phi}{\partial x^2} + D_{yy} \frac{\partial^2 \phi}{\partial y^2} - v_x \frac{\partial \phi}{\partial x} - v_y \frac{\partial \phi}{\partial y} \right] \right] \cdot \{ \mathbf{c}^{t+1} \} \\ & = \left[\frac{1}{\Delta t} + (1 - \theta) \cdot \left[D_{xx} \frac{\partial^2 \phi}{\partial x^2} + D_{yy} \frac{\partial^2 \phi}{\partial y^2} - v_x \frac{\partial \phi}{\partial x} - v_y \frac{\partial \phi}{\partial y} \right] \right] \cdot \{ \mathbf{c}^t \} \end{aligned} \quad (17)$$

In this study, the Crank–Nicolson method is applied by setting the parameter $\theta = 0.5$. Eqs. (16) and (17) apply to all the internal nodes. The governing equations, combined with boundary conditions, are assembled into a global matrix–vector system of the form $\mathbf{A}_h \cdot \mathbf{h}^{t+\Delta t} = \mathbf{B}_h$ and $\mathbf{A}_c \cdot \mathbf{c}^{t+\Delta t} = \mathbf{B}_c$ for flow and transport model respectively. The unknown head h and concentration C at each node is computed using its local support domain, resulting in a sparse global matrix \mathbf{A} . The vector \mathbf{B} includes the source term associated with source/sink terms.

3.3 EFGM Formulation

EFGM uses Galerkin integral approach. In EFGM, the integral form of a governing equation weighted with the MLS shape functions gives a set of linear algebraic equations. This study uses cubic spline weight function and rectangular influence domain to compute the MLS shape functions. Further, dimensionless factor (α_i) of 1 is used to define the influence domain size given by $d_{mx} = \alpha_i \Delta x$ and $d_{my} = \alpha_i \Delta y$ for x and y directions, respectively. The EFGM procedure to discretize the governing groundwater flow and contaminant transport equations can be referred to [38,44]. EFGM formulation of groundwater flow equation is given by:

$$\int_{\Omega} \left(\frac{\partial}{\partial x} \left(K_x h \frac{\partial h}{\partial x} \right) + \frac{\partial}{\partial y} \left(K_y h \frac{\partial h}{\partial y} \right) - \left(S_y \frac{\partial h}{\partial t} \right) \pm Q + q \right) \Phi d\Omega = 0 \quad (18)$$

On using the trial function $h(x, y, t) = \sum_{I=1}^n h_I(t) \phi_I(x, y)$ shape function $\Phi(x, y) = [\phi_1(x, y) \ \phi_2(x, y) \ \phi_3(x, y) \ \dots \ \phi_n(x, y)]$, and $\frac{\partial h}{\partial t} = \left(\frac{h_I^{t+\Delta t} - h_I^t}{\Delta t} \right)$, Eq. (18) becomes

$$\begin{aligned} & \int_{\Omega} \left(K_x h_I^t \frac{\partial \phi_I(x, y)}{\partial x} \frac{\partial \phi_J(x, y)}{\partial x} \right) h_I^{t+\Delta t} d\Omega + \int_{\Omega} \left(K_y h_I^t \frac{\partial \phi_I(x, y)}{\partial y} \frac{\partial \phi_J(x, y)}{\partial y} \right) h_I^{t+\Delta t} d\Omega \\ & + \int_{\Omega} \left(S_y \phi_I(x, y) \phi_J(x, y) \left(\frac{h_I^{t+\Delta t} - h_I^t}{\Delta t} \right) \right) d\Omega \\ & \pm \int_{\Omega} Q_I \phi_I(x, y) \phi_J(x, y) d\Omega - \int_{\Omega} q_I(x, y) \phi_J(x, y) d\Omega \\ & = q_B \int_{\Gamma_E} q_I(x, y) \phi_J(x, y) d\Omega \end{aligned} \quad (19)$$

In Eq. (19), I and J varies from 1 to the number of local nodes (n) within the influence domain of point of interest, q_B is boundary flux and Γ_E is flux boundary. The integral expressions in Eq. (19) are calculated through the Gaussian quadrature method and local matrices are obtained for each of the integral on the left-hand side. These local matrices are then assembled into respective global matrices which are gathered to get the resultant global matrix $[\mathbf{G}_H]$. The indices I and J takes global number from 1 to total meshless nodes (N) while assembling global matrices. Finally, derived system of equations is solved to obtain the head at all meshless nodes i.e., $\{ \mathbf{h}_I^{t+\Delta t} \}$ at time step $(t + \Delta t)$,

$$[\mathbf{G}_H] \{ \mathbf{h}_I^{t+\Delta t} \} = \{ \mathbf{f}_I \} \quad (20)$$

where $\{f_I\}$ is a flux vector consisting of imposed boundary conditions and source/sink term. To apply the Dirichlet boundary conditions, Eq. (20) uses the penalty method as given in [38]. Next, EFGM formulation of contaminant transport equation is given by

$$\int_{\Omega} \left(\frac{\partial}{\partial x} \left(D_{xx} \frac{\partial c}{\partial x} \right) + \frac{\partial}{\partial y} \left(D_{yy} \frac{\partial c}{\partial y} \right) - \frac{\partial (v_x c)}{\partial x} - \frac{\partial (v_y c)}{\partial y} - \frac{\partial c}{\partial t} \right) \Phi d\Omega = 0 \quad (21)$$

On applying EFGM steps to Eq. (21), the following system of equation can be obtained like Eq. (20) for head and solved to get the concentration for the next time step i.e., $\{c_I^{t+\Delta t}\}$ [44]:

$$[\mathbf{G}_C] \{c_I^{t+\Delta t}\} = \{c_{fI}\} \quad (22)$$

3.4 MLPG Formulation

The weak forms of meshless methods usually use a background mesh for integration. The global weak form methods have this issue, which do not make them truly Meshless methods. In MLPG, the integration is done using overlapping of local sub domains. Thus, the MLPG does not need background mesh in any stages of integration and interpolation, which makes it a truly meshless method. In the MLPG method, let the sub-domain be denoted by Ω_s with its area and boundary represented by $\partial\Omega_s$ and A_{Ω_s} . The radius of each sub-domain is taken as 0.3 to 0.8 times the nodal spacing to prevent the overlap of neighboring sub-domain boundaries. In the present study, the MLPG5 formulation is adopted, in which the governing equation is multiplied by a Heaviside step function. This formulation effectively removes the singular and domain integral terms, resulting in a solution that is stable, accurate, and computationally efficient [48]. The time derivative is discretized using the implicit Crank–Nicolson scheme which is known for its numerical stability. Since this method requires an average of the unknown variables at the present and subsequent time steps, the relaxation parameter θ is taken as 0.5. Let Δt denote the time step, t and $t + 1$ represent the current and next time steps, respectively. The resulting MLPG formulation for groundwater flow in an unconfined aquifer is expressed as [41]:

$$\mathbf{A}_h \{h^{t+1}\} = \mathbf{B}_h \quad (23)$$

where,

$$\mathbf{A}_h = \int_{\Omega_s} \frac{S_y}{\Delta t} d\Omega - \left(\int_{\partial\Omega_s} \left(K_x \frac{\partial \Phi}{\partial x} n_x + K_y \frac{\partial \Phi}{\partial y} n_y \right) \{h^{t+1}\} d\Gamma \right) \theta \quad (24)$$

$$\mathbf{B}_h = qA_{\Omega_s} \mp Q + \left[\int_{\Omega_s} \frac{S_y}{\Delta t} d\Omega + \left(\int_{\partial\Omega_s} \left(K_x \frac{\partial \Phi}{\partial x} n_x + K_y \frac{\partial \Phi}{\partial y} n_y \right) \{h^t\} d\Gamma \right) (1 - \theta) \right] \hat{h}^t \quad (25)$$

Using a penalty factor of α , at the Dirichlet boundary:

$$\alpha \int_{\partial\Omega_s} \Phi \hat{h} d\Gamma = \alpha \int_{\partial\Omega_s} \Phi h_1 d\Gamma \quad (26)$$

The Neumann boundary condition is applied directly as:

$$\int_{\partial\Omega_s} \Phi K_n \frac{\partial h}{\partial n} d\Gamma = \int_{\partial\Omega_s} \Phi f_1 d\Gamma \quad (27)$$

here, n represents the normal direction, h_1 and f_1 are the constant head at Dirichlet boundary and constant flux at the Neumann boundary.

Similarly, the MLPG formulation for contaminant transport can be written as [41]:

$$\mathbf{A}_c \{\hat{\mathbf{c}}^{t+1}\} = \mathbf{B}_c \quad (28)$$

where,

$$\mathbf{A}_c = \left(\int_{\Omega_s} \frac{1}{\Delta t} d\Omega - \left(\int_{\partial\Omega_s} \left(D_{xx} \frac{\partial\Phi}{\partial x} n_x + D_{yy} \frac{\partial\Phi}{\partial y} n_y \right) d\Gamma - \int_{\Omega_s} \left(v_x \frac{\partial\Phi}{\partial x} + v_y \frac{\partial\Phi}{\partial y} \right) d\Omega \right) \theta \right) \quad (29)$$

$$\mathbf{B}_c = \left(\int_{\Omega_s} \frac{1}{\Delta t} d\Omega + \left(\int_{\partial\Omega_s} \left(D_{xx} \frac{\partial\Phi}{\partial x} n_x + D_{yy} \frac{\partial\Phi}{\partial y} n_y \right) d\Gamma - \int_{\Omega_s} \left(v_x \frac{\partial\Phi}{\partial x} + v_y \frac{\partial\Phi}{\partial y} \right) d\Omega \right) (1 - \theta) \right) \hat{\mathbf{c}}^t \quad (30)$$

The Dirichlet and Neumann boundary conditions are given as:

$$\alpha \int_{\partial\Omega_s} \Phi \hat{c}_j d\Gamma = \alpha \int_{\partial\Omega_s} \Phi c_1 d\Gamma \quad (31)$$

$$\int_{\partial\Omega_s} \left(D_{xx} \frac{\partial\Phi}{\partial x} n_x + D_{yy} \frac{\partial\Phi}{\partial y} n_y \right) d\Gamma = \int_{\partial\Omega_s} \Phi f_2 d\Gamma \quad (32)$$

where, c_1 and f_2 are the constant concentration and constant concentration flux at Dirichlet and Neumann boundaries, respectively. The MLPG based coupled flow and transport model for unconfined aquifer is developed using the derived equations.

4 Modelling Procedure

The developed RPCM, EFGM and MLPG models for the aquifer flow is integrated with a transport model to form integrated flow and transport model. The flow chart describing the model is given in Fig. 2. The procedure can be described as follows:

Step 1: The hydrogeological details, problem domain, meshless parameters, number of nodes and the corresponding arrangement, pumping wells, streams, recharge zones, heterogeneity and anisotropy, initial and boundary conditions are inputted into the meshless models.

Step 2: The size of the support and sub domain are fixed. The sub domain is used for the integration of the MLPG and EFGM models. The support domain is used for the interpolation.

Step 3: The meshless formulations for groundwater flow equation are solved using MATLAB and Python for solving the unknown head values. The RPCM model was developed in Python, while the EFGM and MLPG models were developed in MATLAB. Consistent numerical procedures and solver parameters were maintained across the platforms to ensure comparability of results.

Step 4: The velocity is calculated using the Darcy's law and the dispersion coefficients are computed using Eqs. (9) and (10).

Step 5: The values computed in step 4 are inputted into the transport model. The meshless transport models are implemented, similar to step 4 and the contamination concentration are computed.

Step 6: The steps 3, 4 and 5 are repeated.

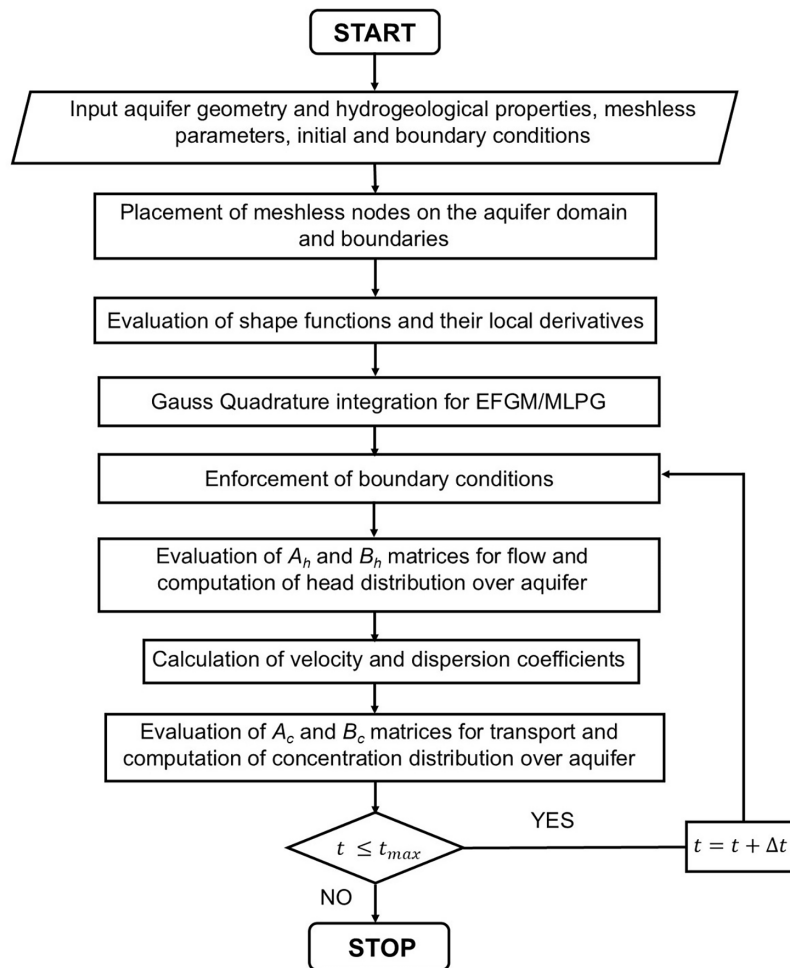


Figure 2: Modelling procedure of meshless based coupled flow and transport models.

5 Case Studies

5.1 Case Study 1

A hypothetical square-shaped confined aquifer with dimensions of $1400 \text{ m} \times 1400 \text{ m}$ is considered (Fig. 3a) for validating and comparing the meshless models. Constant boundary conditions of 100 m are imposed along the left and right boundaries, while the top and bottom boundaries are treated as no-flow boundaries. The aquifer transmissivity and storativity are taken as $100 \text{ m}^2/\text{day}$ and 0.001, respectively. A pumping well is located at the center of the domain, with a pumping rate of $10,000 \text{ m}^3/\text{day}$. The domain is discretized into 225 nodes, and six locations are designated as observation points, as shown in Fig. 3a. The head distribution simulated using the meshless models are compared with the analytical solution proposed by Willis and Yeh [49] at the selected observation wells given in Fig. 3a. The results are presented in Table 1. The head distribution obtained from the MLPG model is illustrated in Fig. 3b, while the other meshless models exhibit identical contour patterns. As evident from the results in Table 1, all meshless models show excellent agreement with the analytical solution. The average errors at the six observation wells are 1.25%, 0.666%, 0.442% and 0.16% for MODFLOW, RPCM, MLPG and EFGM models, respectively. These results establish the reliable performance of all the three meshless models, with the EFGM model showing higher accuracy.

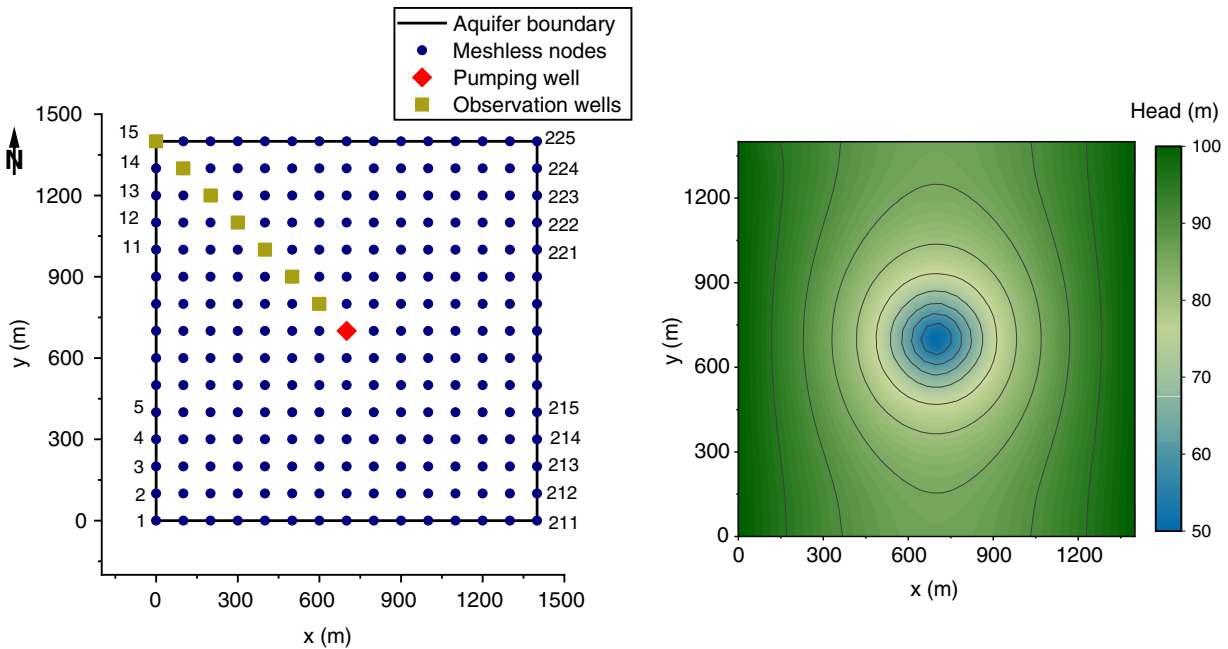


Figure 3: Case study 1 (a) nodal arrangement and (b) head distribution from MLPG model.

Table 1: Comparison of head values obtained from meshless models with analytical solution.

| Node Number | Analytical Solution (m) | MODFLOW | | RPCM | | MLPG | | EFGM | |
|-------------|-------------------------|----------|-----------|----------|-----------|----------|-----------|----------|-----------|
| | | Head (m) | Error (%) | Head (m) | Error (%) | Head (m) | Error (%) | Head (m) | Error (%) |
| 29 | 97.01 | 98.04 | 1.06 | 97.82 | 0.83 | 97.00 | 0.01 | 96.98 | 0.03 |
| 43 | 93.80 | 94.04 | 0.25 | 93.27 | 0.57 | 93.84 | 0.04 | 93.74 | 0.06 |
| 57 | 90.09 | 91.20 | 1.23 | 90.10 | 0.01 | 91.55 | 1.62 | 89.99 | 0.11 |
| 71 | 85.45 | 86.10 | 0.76 | 85.50 | 0.06 | 85.70 | 0.29 | 85.31 | 0.16 |
| 85 | 78.98 | 80.14 | 1.46 | 79.51 | 0.67 | 79.43 | 0.57 | 78.77 | 0.27 |
| 99 | 67.95 | 69.80 | 2.72 | 69.21 | 1.85 | 68.03 | 0.12 | 67.73 | 0.32 |

5.2 Case Study 2

In this case study, the three meshless models are applied to a hypothetical unconfined aquifer with an irregular boundary geometry [50]. The aquifer extends 290 m in the x direction and 190 m in the y direction, as shown in Fig. 4a. The aquifer is bounded by Dirichlet boundary on the West and East, with constant head values of 132 and 128 m. The remaining boundaries are considered to be no flow boundaries.

The aquifer is assumed to be homogeneous and isotropic, with a hydraulic conductivity of 5 m/day and an effective porosity of 0.3. Three pumping wells are located at node numbers 76, 294, and 442, each operating at a rate of 200 m³/day. Three recharge wells are located at node numbers 68, 283, and 449, each recharging at a rate of 200 m³/day. A constant Total Dissolved Solids (TDS) concentration of 500 mg/L is introduced at node number 130. The models are simulated over a period of 2 years using a time step of one day to evaluate contaminant concentrations. For meshless simulation, the aquifer domain was discretized using 514 nodes, as shown in Fig. 4b.

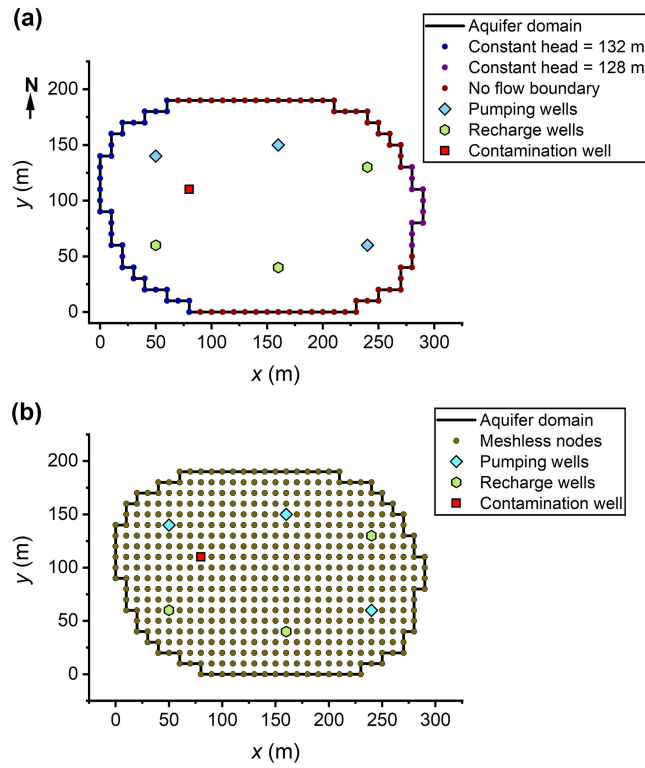


Figure 4: (a) Problem domain, (b) Meshless nodal distribution for the hypothetical case study.

Since no analytical solution is available for this case study, a coupled MODFLOW and MT3DMS model is used as a reference rather than for intercomparison. The MODFLOW-MT3DMS model is developed with a uniform grid size of 10 m × 10 m. The performance of the meshless models is evaluated against MODFLOW and MT3DMS using multiple statistical indicators, including average error, Root Mean Square Error (RMSE), Normalized Root Mean Square Error (NRMSE), Nash–Sutcliffe Efficiency (NSE) and L_∞ error given by the following equations:

$$\text{Average error (\%)} = 100 \left(\frac{1}{N_{obs}} \sum_{nn=1}^{N_{obs}} |h_{nn}^{obs} - h_{nn}^{sim}| \right) \quad (33)$$

$$\text{RMSE} = \sqrt{\frac{\sum_{nn=1}^{N_{obs}} (h_{nn}^{obs} - h_{nn}^{sim})^2}{N_{obs}}} \quad (34)$$

$$\text{NRMSE} = 100 * \frac{\text{RMSE}}{h_{average}^{obs}} \quad (35)$$

$$\text{NSE} = 1 - \frac{\sum_{nn=1}^{N_{obs}} (h_{nn}^{obs} - h_{nn}^{sim})^2}{\sum_{nn=1}^{N_{obs}} (h_{nn}^{obs} - h_{n_{average}}^{obs})^2} \quad (36)$$

$$L_\infty \text{ error} = \max_{1 \leq nn \leq N_{obs}} (|h_{nn}^{obs} - h_{nn}^{sim}|) \quad (37)$$

In the Eqs. (32)–(36), N_{obs} is the number of observation wells, h_{nn}^{obs} and h_{nn}^{sim} are the actual head and the simulated head at the observation well and $h_{average}^{obs}$ is the average of actual head values.

The flow models are first executed, and the steady-state hydraulic head contours obtained from MODFLOW, RPCM, MLPG and EFGM are given in Fig. 5. The local support domain sizes are taken as 3 times the nodal distance for RPCM and MLPG models. The RPCM model parameters which include the MQ-RBF shape parameters i.e., q and α are set as 0.98 and 5, respectively, from the previous literature [39]. The sub-domain size is taken as 0.45 times the nodal spacing in MLPG model [41]. The dimensionless size of the influence domain α_i of EFGM is taken as 1. The groundwater head values comparison at twelve points are provided in Tables 2 and 3. The results reveal close agreement between the meshless models and the MODFLOW solutions. Further, heads from the flow model are used to compute nodal velocities and dispersion coefficients, which are then used as inputs to the transport model.

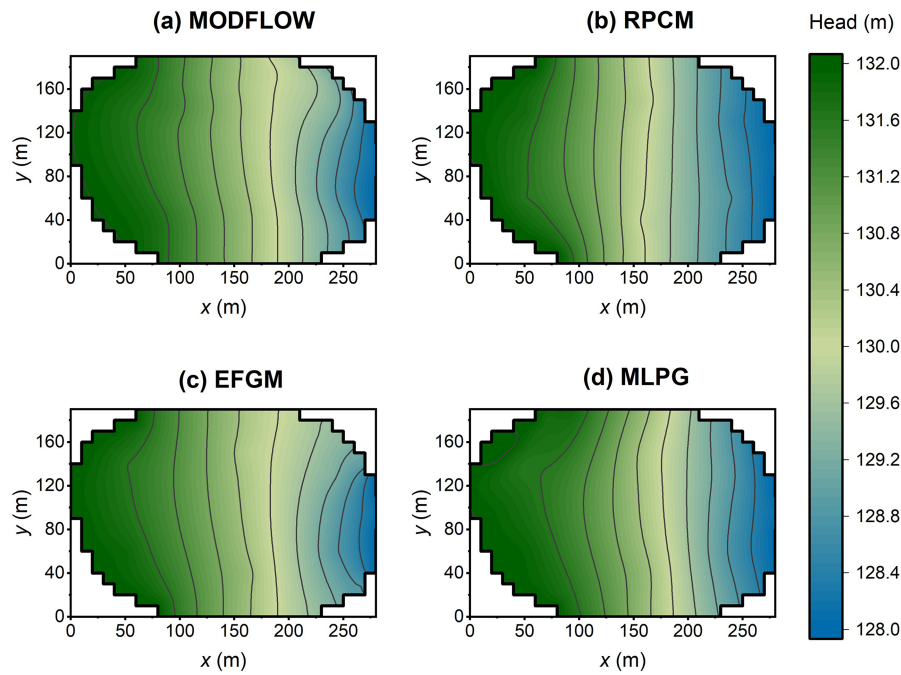


Figure 5: Distribution of the groundwater head from the four models for hypothetical aquifer.

Table 2: Comparison of groundwater head from the meshless models with MODFLOW for the hypothetical case study.

| Location (m) | MODFLOW-Head (m) | RPCM | | EFGM | | MLPG | |
|--------------|------------------|----------|-----------|----------|-----------|----------|-----------|
| | | Head (m) | Error (%) | Head (m) | Error (%) | Head (m) | Error (%) |
| (20, 70) | 131.985 | 131.952 | 0.025 | 131.963 | 0.017 | 131.980 | 0.004 |
| (30, 100) | 131.870 | 131.823 | 0.035 | 131.837 | 0.025 | 131.883 | 0.010 |
| (110, 40) | 131.277 | 130.976 | 0.229 | 131.205 | 0.055 | 131.297 | 0.016 |
| (120, 150) | 130.972 | 130.747 | 0.172 | 130.865 | 0.082 | 131.088 | 0.089 |
| (140, 140) | 130.670 | 130.423 | 0.189 | 130.572 | 0.075 | 130.662 | 0.006 |
| (170, 150) | 130.165 | 129.948 | 0.167 | 130.144 | 0.016 | 130.098 | 0.052 |
| (190, 190) | 129.816 | 129.525 | 0.224 | 130.007 | 0.147 | 129.868 | 0.040 |
| (210, 10) | 129.643 | 129.182 | 0.355 | 129.688 | 0.035 | 129.521 | 0.093 |
| (230, 80) | 129.109 | 128.874 | 0.182 | 129.157 | 0.037 | 128.949 | 0.123 |

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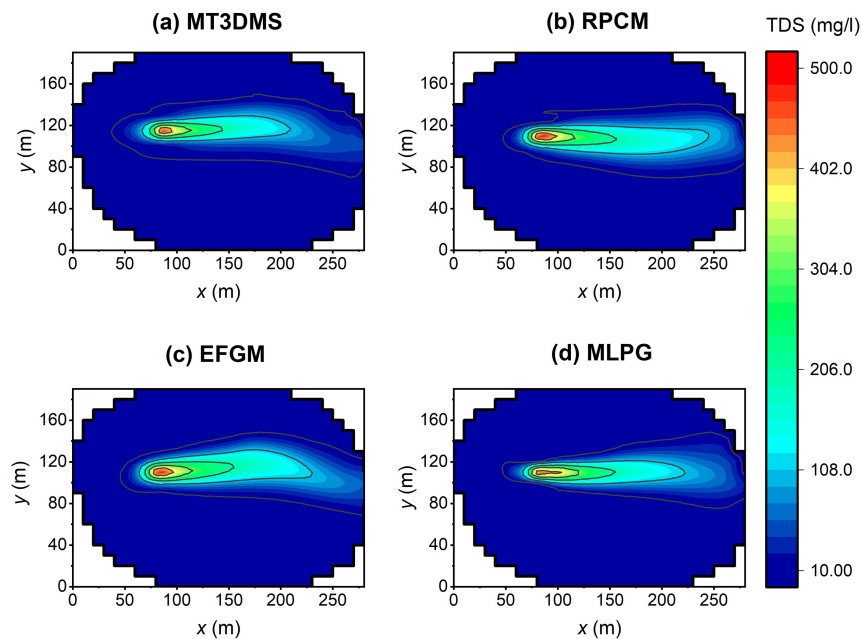
Table 2 (continued)

| Location (m) | MODFLOW-Head (m) | RPCM | | EFGM | | MLPG | |
|--------------|------------------|----------|-----------|----------|-----------|----------|-----------|
| | | Head (m) | Error (%) | Head (m) | Error (%) | Head (m) | Error (%) |
| (250, 10) | 128.924 | 128.540 | 0.298 | 129.169 | 0.190 | 128.744 | 0.139 |
| (260, 120) | 128.616 | 128.297 | 0.248 | 128.715 | 0.077 | 128.422 | 0.151 |
| (280, 90) | 128.079 | 128.053 | 0.020 | 128.131 | 0.040 | 128.106 | 0.021 |

Table 3: Comparison of difference with respect to MODFLOW for different meshless models for case study 1.

| | RPCM | EFGM | MLPG |
|------------------------|-------|-------|-------|
| Average error (%) | 0.179 | 0.066 | 0.062 |
| RMSE | 0.267 | 0.109 | 0.105 |
| NRMSE (%) | 0.205 | 0.083 | 0.080 |
| NSE | 0.999 | 0.999 | 0.999 |
| L_{∞} error (m) | 0.461 | 0.245 | 0.194 |

The concentration contours after 2 years are estimated and plotted as shown in Fig. 6. The breakthrough curves, representing the variation of concentration over the simulation time, at nodes 170, 190, 210 and 230 are shown in Fig. 7. As observed from these plots, there is close agreement among the RPCM, EFGM, MLPG and MT3DMS models. Thus, the proposed meshless models are demonstrated to be reliable for simulating the flow and transport in the porous media.

**Figure 6:** Concentration distribution after 2 years from the four models for the hypothetical aquifer.

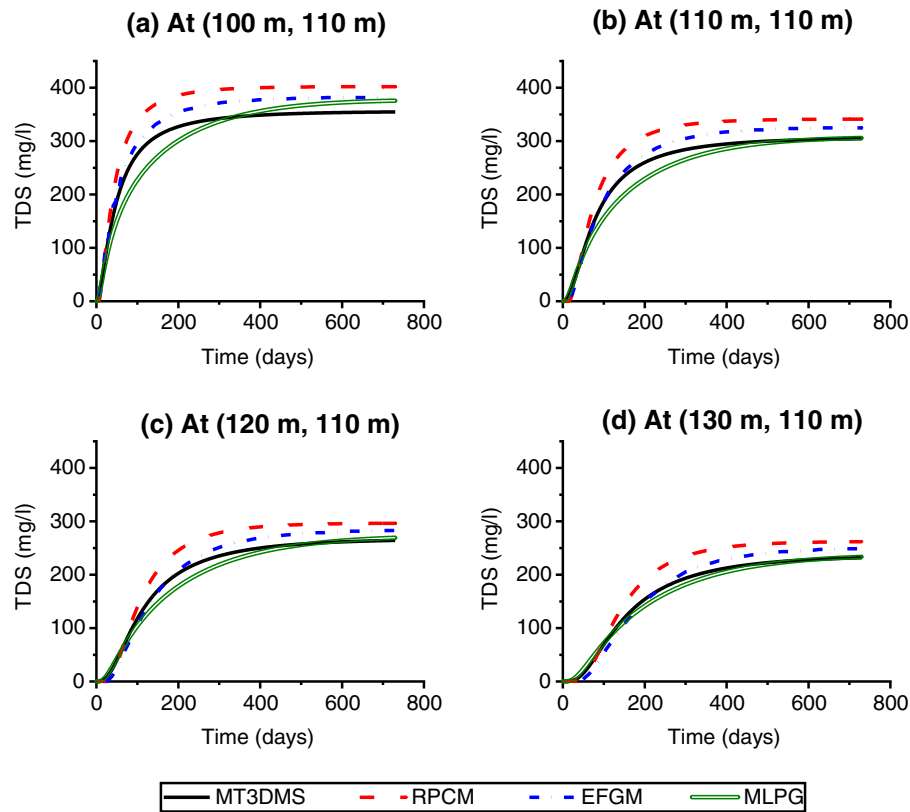


Figure 7: Breakthrough curves at four nodes (a) Node 170 (b) Node 190 (c) Node 210 and (d) Node 230 from the four models for case study 2.

As meshless parameters strongly influence the model performance, a sensitivity analysis is conducted. The RBF shape parameters q and α of the RPCM model are varied around the base case ($q = 0.98$, $\alpha = 5$) with $q = 0.5$ and $\alpha = 1, 2, 3$, and 7 . Similarly, support domain size of EFGM, support and sub domain radii of MLPG are varied as 0.3 and 0.45 to demonstrate the model performance under varying meshless parameters. The results as shown in Fig. 8a show that the transport solution is more sensitive to reduction in q , which increases numerical diffusion and alter breakthrough behavior, whereas moderate variations in α produce comparatively smaller deviations. From Fig. 8b,c, it can be observed that solutions are stable within a recommended parameter range [38,51]. In addition, the three meshless models are tested under varying time steps of 0.5 day, 1 day and 2 days, as shown in Fig. 8d–f. The solutions remain stable for time steps up to $\Delta t = 2$ days, as shown in the breakthrough curves at four observation nodes. Thus, this analysis aids in parameter selection and demonstrates the robustness of the models within the recommended ranges [38,39,51]. However, model sensitivity outside these ranges can significantly impact the performance, often necessitating a trial-and-error approach for optimal parameter calibrations.

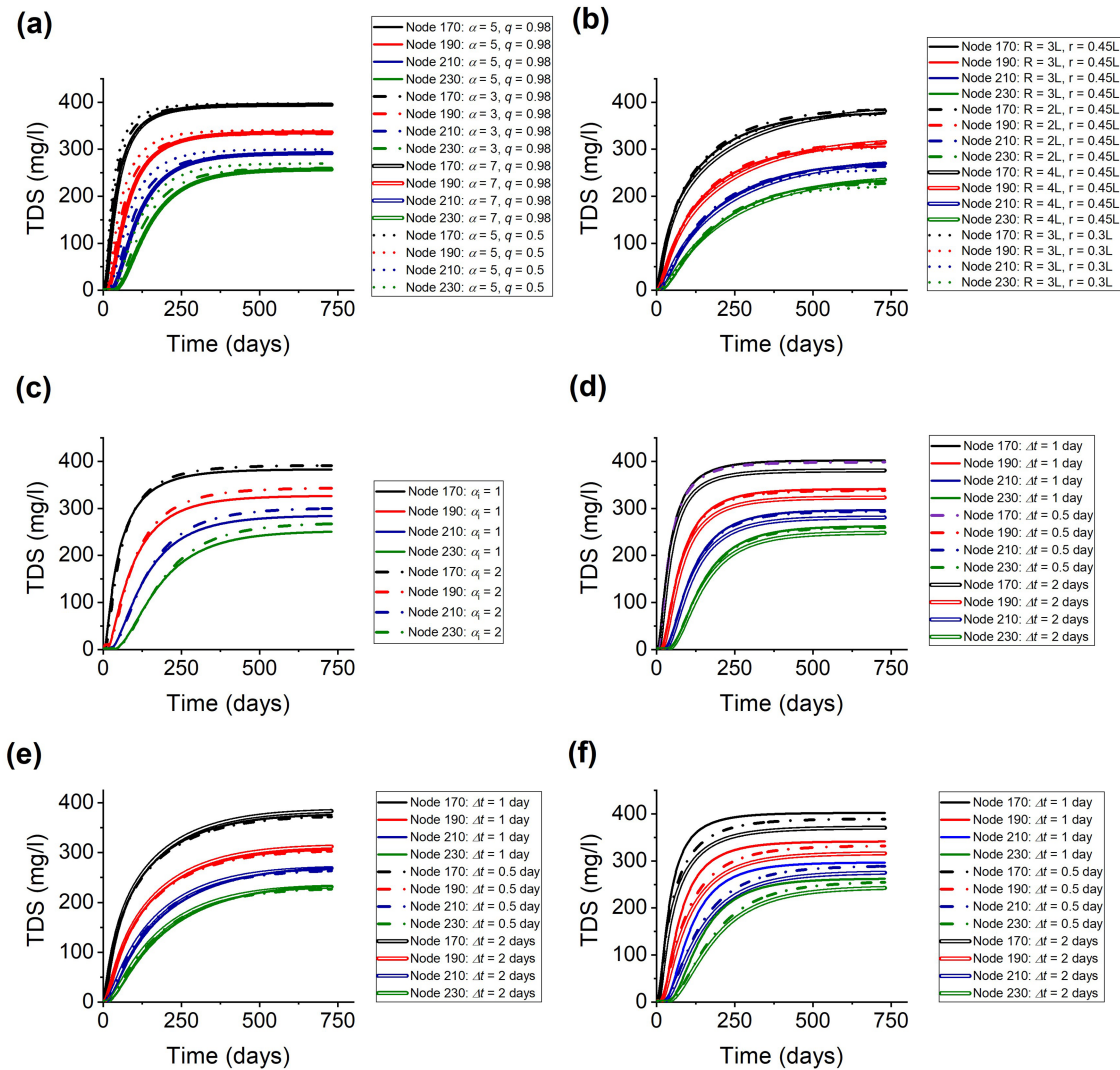


Figure 8: Performance of the meshless models under varying parameters. (a) RPCM model response to variations in RBF shape parameters, (b) MLPG model response to changes in the ratios of support domain radius (R) and sub-domain radius (r) relative to nodal spacing (L), (c) EFGM model response to variations in size of the influence domain (α_i), (d) RPCM model performance under varying time steps, (e) MLPG model performance under varying time steps, (f) EFGM model performance under varying time steps.

5.3 Case Study 3

To evaluate the applicability of meshless methods for large-scale field problems, the RPCM, EFGM and MLPG models are applied to a large, field unconfined aquifer located in the Patancheru industrial development area of Telangana, India for groundwater flow simulation (Fig. 9). The site information details are available in [52,53].

The study area contains two streams, Nakkavagu and Pedhavagu, and a comprehensive groundwater level monitoring was conducted in this area during 1997 [52]. The area of the aquifer is approximately 93 km^2 and its thickness is 15 m. All the boundaries of domain are Neumann boundaries with zero flux. There are 15 observation wells in the aquifer. The aquifer domain is illustrated in Fig. 9. The groundwater recharge is taken from precipitation of 110 mm/year, and the seepage from the stream is considered to be 130 mm/year.

The initial value of hydraulic conductivity of 62.5 m/day is modified to 60 m/day during the calibration for improved model accuracy. There are 189 bore wells in the study area, each extracting groundwater at a rate of 95 m³/d and operating for 60% of the day [53].

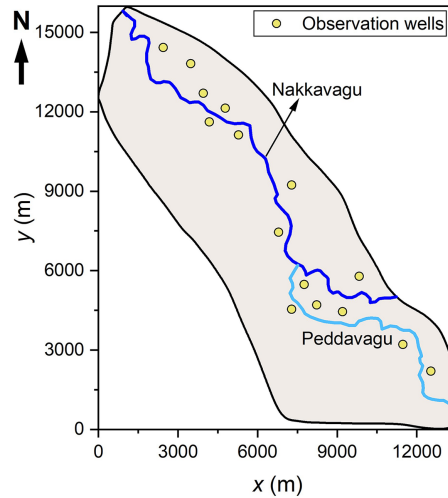


Figure 9: Problem domain of the field-scale study.

A uniformly distributed arrangement of 1597 nodes with 250 m nodal spacing are considered for the meshless simulation. The meshless model parameters are kept similar to the case study 2. The spatial distribution of meshless nodes and the locations of the bore wells are shown in Fig. 10.

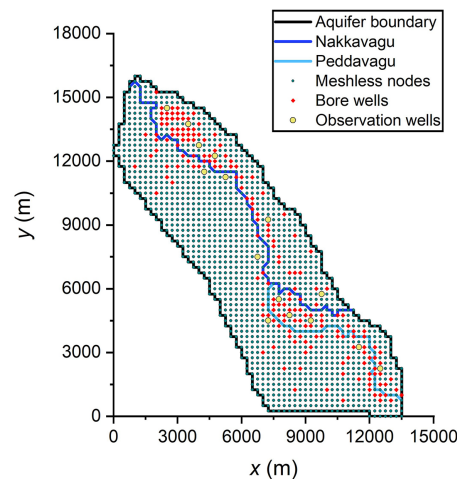


Figure 10: Meshless nodal arrangement for the field-scale case study using MODFLOW, RPCM, EFGM and MLPG models.

The meshless flow models for unconfined aquifer are first executed to obtain a steady state head distribution for the year 1997. The velocities over the aquifer domain are computed using Darcy’s law given in Eq. (9). The simulated head values obtained from the meshless model are compared with observed head values [52]. Additionally, widely used MODFLOW is applied to establish a reference model for transient state simulation, rather than for direct comparison of meshless solutions. The solutions are assessed using average error, RMSE, NRMSE, NSE and L_{∞} error.

The contour plots of the head distribution are shown in Fig. 11 using the MODFLOW, RPCM, EFGM and MLPG models. The flow direction is observed to be from the southeast to the northwest, following the gradient from higher to lower hydraulic heads. The comparison of head at observation wells from MODFLOW and meshless models with the actual head values are given in Tables 4 and 5. It can be observed that meshless solutions are in excellent agreement with the observed head values and are slightly more accurate than the MODFLOW model. The low average error, RMSE, NRMSE, L_∞ error and NSE values are closer to 1 indicating the effectiveness of the MLPG flow simulation model. Additionally, the meshless model has better reusability due to easier adaptive analysis.

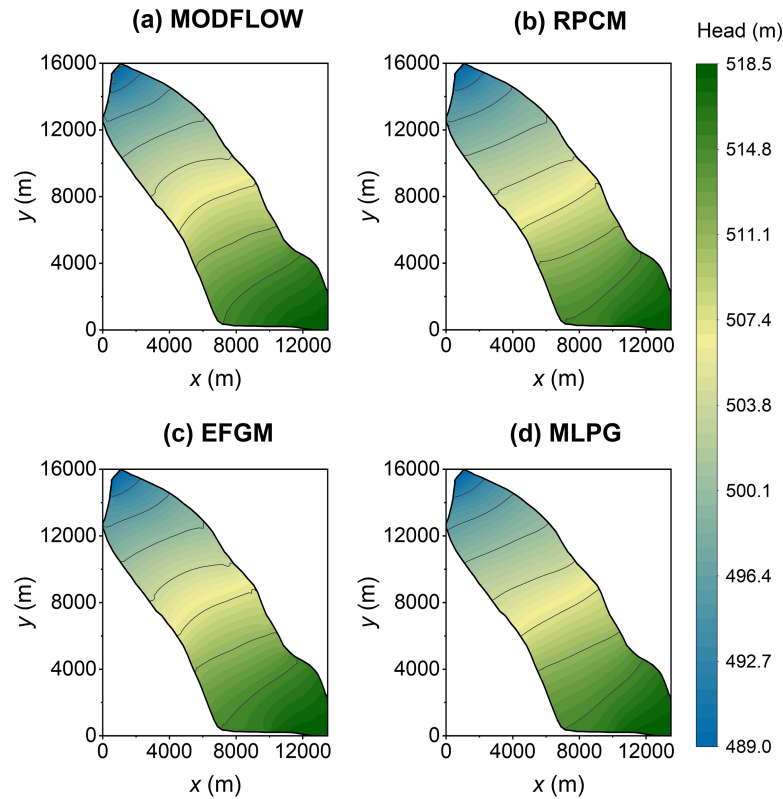


Figure 11: Groundwater head distribution in 1997 using MODFLOW, RPCM, EFGM and MLPG models.

Table 4: Comparison of simulated steady state head values with the observed head in 1997.

| Location of Observation Well (m) | Observed Head (m) | MODFLOW | | RPCM | | EFGM | | MLPG | |
|----------------------------------|-------------------|----------|-----------|----------|-----------|----------|-----------|----------|-----------|
| | | Head (m) | Error (%) | Head (m) | Error (%) | Head (m) | Error (%) | Head (m) | Error (%) |
| (2500, 14,500) | 494.012 | 494.864 | 0.172 | 494.551 | 0.109 | 494.5672 | 0.112 | 494.492 | 0.097 |
| (3500, 13,750) | 495.200 | 497.153 | 0.394 | 496.770 | 0.317 | 496.8018 | 0.323 | 496.780 | 0.319 |
| (4000, 12,750) | 498.562 | 499.346 | 0.157 | 498.528 | 0.007 | 498.7867 | 0.045 | 498.827 | 0.053 |
| (4750, 12,250) | 499.881 | 500.389 | 0.102 | 499.658 | 0.045 | 499.9832 | 0.020 | 500.049 | 0.034 |
| (5250, 11,250) | 504.163 | 502.129 | 0.403 | 501.209 | 0.586 | 501.7823 | 0.472 | 501.875 | 0.454 |
| (7250, 9250) | 505.749 | 505.724 | 0.005 | 505.120 | 0.124 | 505.6084 | 0.028 | 505.684 | 0.013 |
| (6750, 7500) | 506.605 | 508.502 | 0.375 | 507.053 | 0.088 | 507.8803 | 0.252 | 508.004 | 0.276 |

(Continued)

Table 4 (continued)

| Location of Observation Well (m) | Observed Head (m) | MODFLOW | | RPCM | | EFGM | | MLPG | |
|----------------------------------|-------------------|----------|-----------|----------|-----------|----------|-----------|----------|-----------|
| | | Head (m) | Error (%) | Head (m) | Error (%) | Head (m) | Error (%) | Head (m) | Error (%) |
| (7750, 5500) | 509.242 | 511.738 | 0.490 | 510.191 | 0.186 | 510.75 | 0.296 | 510.844 | 0.315 |
| (9750, 5750) | 509.502 | 511.735 | 0.438 | 511.252 | 0.343 | 511.2536 | 0.344 | 511.543 | 0.401 |
| (7250, 4500) | 511.285 | 512.510 | 0.239 | 511.132 | 0.030 | 511.6463 | 0.071 | 511.742 | 0.089 |
| (8250, 4750) | 512.139 | 512.975 | 0.163 | 511.386 | 0.147 | 511.8838 | 0.050 | 511.991 | 0.029 |
| (9250, 4500) | 513.458 | 513.747 | 0.056 | 512.336 | 0.219 | 512.7881 | 0.130 | 512.896 | 0.109 |
| (11,500, 3250) | 514.248 | 516.149 | 0.369 | 515.437 | 0.231 | 515.5208 | 0.248 | 515.729 | 0.288 |
| (12,500, 2250) | 516.291 | 517.309 | 0.197 | 516.947 | 0.127 | 517.0441 | 0.146 | 517.082 | 0.153 |

Table 5: Comparison of errors for different models.

| | MODFLOW | RPCM | EFGM | MLPG |
|------------------------|---------|-------|-------|-------|
| Average error (%) | 0.254 | 0.183 | 0.181 | 0.188 |
| RMSE | 2.892 | 1.189 | 1.147 | 2.319 |
| NRMSE (%) | 0.571 | 0.235 | 0.226 | 0.458 |
| NSE | 0.954 | 0.588 | 0.973 | 0.970 |
| L_{∞} error (m) | 2.496 | 2.954 | 2.381 | 2.288 |

Subsequently, RPCM, EFGM and MLPG flow models are executed in transient state conditions, and head distribution in 2025 is generated. Thus, the transient state models are executed for 28 years, with a time step of 14 days, with an assumption that the stress remains constant. The MODFLOW simulation is implemented with the same parameters. The head distributions in 2025 obtained from the MODFLOW, RPCM, EFGM and MLPG models are shown in Fig. 12. The meshless solutions indicate a closer similarity among the meshless models and MODFLOW. Also, head distribution in 2025 is close to that in 1997, due to the constant minimal stresses and attainment of steady state under the assumed conditions.

Further, high pumping rate of 3000 m³/day is considered at each of the pumping wells to evaluate the model response under hypothetical transient stressed conditions. Using the 2025 head distribution as the initial condition, transient simulations are run for one-year period. The value of α_i is taken as 2. As shown in Fig. 13, meshless model results are in close agreement with the standard MODFLOW model simulations.

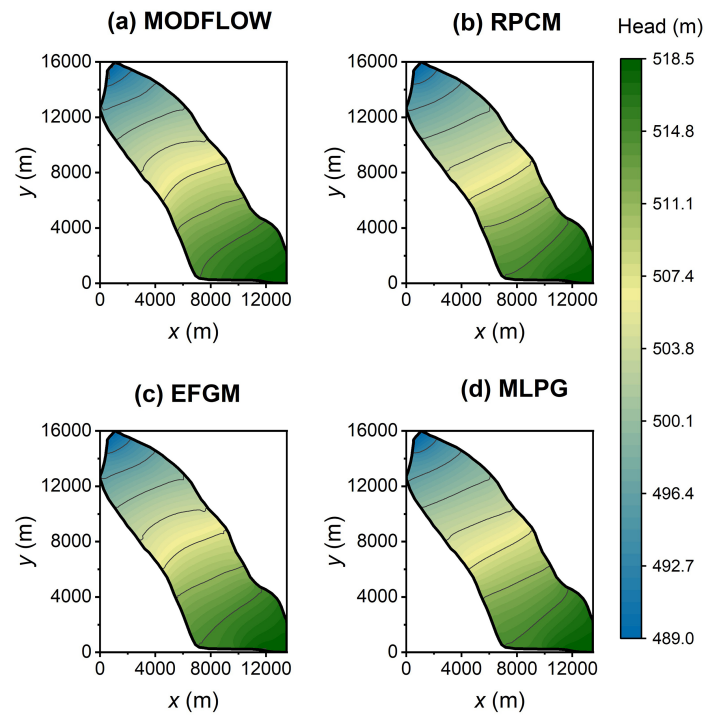


Figure 12: Groundwater head distribution in 2025 using four models.

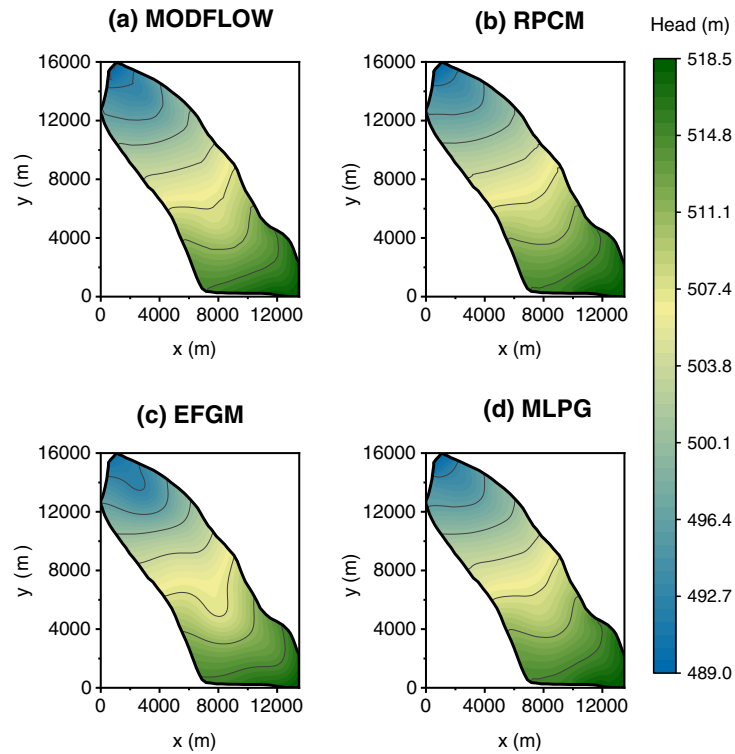


Figure 13: Groundwater head distribution under hypothetical stressed conditions using four models.

6 Discussion

In this study, the performance and efficiency of three categories of meshless methods are evaluated for the simulation of groundwater flow and transport processes. The RPCM, EFGM and MLPG based flow and transport models, previously developed by the authors [39,41,44], are applied to three representative case studies and their results are systematically intercompared. The widely used grid-based MODFLOW-MT3DMS model is adopted as a reference model and implemented using similar spatial and temporal discretization to ensure consistency in comparison.

In the first case study, model results are compared with an analytical solution, and all three meshless models show excellent agreement with the EFGM model providing the highest accuracy. In the second case study, involving a hypothetical unconfined aquifer with an irregular boundary, the MODFLOW-MT3DMS, RPCM, EFGM, and MLPG models are successfully applied for the simulation of head and TDS concentration over a two year period. Among the meshless models, EFGM and MLPG exhibit the closest agreement with MODFLOW results, with average head deviations of 0.062% and 0.066%, respectively. The best overall performance across all statistical evaluation measures is demonstrated by the EFGM model, followed by MLPG model. RPCM model also perform reliably, with an average deviation of 0.179%. The simulated concentration contours after two years indicated good agreement among the four models. However, from the breakthrough curve analysis, an overestimation of concentration values is observed for the EFGM and RPCM models, whereas a slight deviation in the contaminant trend is observed for MLPG model at certain observation points. With respect to computational efficiency, simulations conducted on a Windows 10 platform with an Intel i7 processor and 16 GB RAM require approximately 7, 10.44, and 9.21 s for RPCM, EFGM, and MLPG models, respectively. The lower computational cost of RPCM model is associated with its strong-form formulation, whereas the increased simulation time for EFGM and MLPG models arises from numerical integration procedures involved in the simulation. These observations support the first and second hypotheses, as the weak-form EFGM and MLPG models demonstrated improved numerical agreement relative to the strong-form RPCM under irregular boundary conditions and EFGM achieved higher accuracy at the expense of greater computational effort.

In the third case study, the applicability of meshless models is demonstrated using a field-scale aquifer system located in Telangana, India. To facilitate comparison, observed groundwater level data has been used and MODFLOW is used as a reference model for transient state simulation. The aquifer system, covering approximately 93 km² and including 189 borewells and two streams, is used to assess the applicability of the meshless approaches under realistic hydrogeological conditions. The analysis is limited to flow simulation, with the objective of demonstrating large-domain applicability and direct comparison with available observations. For steady-state conditions corresponding to the year 1997, EFGM model demonstrated the best performance, with an average deviation of 0.101%, followed by the RPCM and MLPG models with average deviations of 0.183% and 0.188%, respectively. The MLPG model exhibits lowest L_{∞} error, indicating that maximum pointwise deviation between simulated and observed heads is minimal. The field-scale results provide evidence in support of the third hypothesis, as all three meshless methods are in close agreement with the observed groundwater heads and MODFLOW model under realistic hydrogeological conditions. A steady-state condition is attained under the considered assumptions, with no significant deviation in head values. Further, a hypothetical stressed scenario with high pumping rates is implemented to assess the transient condition. The meshless models' simulations demonstrate close agreement with the MODFLOW results. However, the time-varying pumping and recharge play a critical role in governing real-world groundwater dynamics. While the primary focus of the present work is methodological development and comparative evaluation of meshless modelling approaches under controlled conditions, incorporation of temporally variable stresses is essential for realistic system representation. Coupling the proposed framework

with time-dependent recharge and pumping data would therefore constitute further extension of this research towards practical, real-world applications.

In this study, the characteristics of three meshless methods are demonstrated. RPCM, as a strong form approach, is characterized by low computational cost and reliable performance. However, as previously reported [41] unstable solutions may be encountered in the presence of Neumann boundary conditions for certain nodal arrangements. The weak form methods such as EFGM and MLPG were found to be very effective in dealing with Neumann boundary conditions, supporting the first hypothesis. In the present study, the most accurate results are consistently obtained using EFGM, but it is not truly meshless, and requires a background mesh for numerical integration. MLPG model is found to provide accurate and stable solutions, but increased computational effort is required due to the local integration process. Thus, the findings indicate that formulation significantly influences numerical stability and efficiency, thereby validating the hypothesis-driven framework adopted in this study. For the solution of a particular problem, based on accuracy requirements, and computational efforts, a particular model may be chosen, depending on the familiarity and requirements of the user.

7 Conclusions

In this study, a comprehensive evaluation of three meshless methods of different formulation categories is demonstrated for the simulation of groundwater flow and solute transport processes. The primary focus is to compare the applicability, advantages, and limitations of the meshless approaches. The strong-form RPCM, global weak-form EFGM, and local weak-form MLPG methods are employed for this purpose. The governing equations are formulated directly in RPCM, whereas numerical integration is required for EFGM and MLPG approaches. In EFGM, integration is performed using a background mesh, while local circular subdomains are used for the integration in MLPG.

The proposed models are evaluated using a simple square domain aquifer, a hypothetical aquifer with an irregular boundary and a field-scale aquifer system. In all cases, excellent agreement is observed with the analytical solution and observed groundwater level data. The purpose of the MODFLOW-MT3DMS model in this study is to serve as a reference framework where analytical solutions or observed data are unavailable, rather than to establish superiority or inferiority relative to meshless approaches. Among the three models, EFGM provides higher accuracy but with maximum computational cost. RPCM and MLPG models also provide reliable solutions. For flow simulations, deviations of less than 0.6% are observed for all three meshless models when compared with the analytical solution, observed data and MODFLOW results. EFGM and MLPG are more effective in handling Neumann boundary conditions than RPCM. RPCM is computationally efficient and well suited for the Dirichlet boundary problems. With the requirement of background mesh and numerical integration, EFGM exhibits reduced flexibility compared to RPCM and MLPG. Overall, the results confirm the effectiveness and applicability of the three meshless methods for groundwater flow and transport modelling across both small-scale and large-scale porous media problems.

The following are some of the limitations of the study. The comparative performance of the meshless methods is assessed only for the case studies considered, and variations in the relative performance, particularly between EFGM and MLPG, may arise under different hydrogeological conditions. The meshless models are found to be sensitive to the sizes of the support and subdomains and require tuning to achieve optimal results. In the field-scale case study, some of the adopted assumptions cause simplifying representation of climate variability and anthropogenic influences on the groundwater system. Incorporating time-varying field stresses, ideally through coupling with a hydrological model, represents an important extension of the present work and enables more realistic simulation of transient, real-world groundwater

systems. Nevertheless, the results demonstrate the potential of meshless methods to evolve into reliable groundwater modelling tools, either as standalone approaches or in combination with grid-based models.

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